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Application No. 10/553,689 Amendment Dated: August 21, 2007 Reply to Office Action of March 22, 2007

## Listing of the Claims:

- 1. (Currently Amended) A gas phase olefin polymerization process comprising:
- (1) preparing a solution of a catalyst precursor comprising a mixture of magnesium and titanium compounds, an electron donor and a solvent;
  - (2) adding a filler to the solution from step (1) to form a slurry;
- (3) spray drying the slurry from step (2) at a temperature of 100 to 140°C to form a spray dried precursor;
  - (4) slurrying the spray dried precursor from step (3) in mineral oil,
- (5) partially or fully pre-activating pre-activating the catalyst precursor by contacting the slurry of step (4) with one or more Lewis Acids employing one or more in-line static mixers, wherein the molar ratio of the Lewis Acid to the electron donor in the catalyst precursor is about 0.1:1 to about 0.75:1; and
- (6) transferring the partially or fully activated pre-activated catalyst precursor from step (5) under plug-flow conditions into a gas phase, olefin polymerization reactor and, if the precursor is partially preactivated, adding an additional amount of the activator to the reactor to produce a homogeneous activated catalyst mixture, wherein the catalyst is partially preactivated in step (5) for about 10 minutes to about 60 minutes prior to the transferring step (6), and wherein the density of a polymer comprising ethylene produced according to the process has a density of 0.930 g/cc or more.
- 2. (Currently Amended) The [[A]] gas phase olefin polymerization process of Claim 1, wherein the filler comprises a porous catalyst support, comprising:
- (1) preparing a solution of a catalyst-precursor comprising a mixture of magnesium and titanium compounds, an electron donor and a solvent;
  - (2) adding a porous catalyst support, to the solution from step (1) to form a slurry;
  - (3) drying the slurry-from step (2) to form a solid catalyst precursor;
  - (4) slurrying the solid precursor from step (3) in a viscous inert liquid,
- (5) partially or fully-pre-activating the catalyst-precursor by contacting the slurry of step (4) with one or more Lewis Acids employing one or more in line static mixers, and
- (6) transferring the partially or fully activated precursor from step (5) under plug flow conditions into a gas-phase, elefin polymerization reactor and, if the precursor is partially preactivated, adding an activator to the reactor.

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- 3. (Currently Amended) The process of claim 1 or 2 wherein;
  - 1) the catalyst precursor in step (1) corresponds to the formula:

 $Mg_d(M)(OR)_cX_f(ED)_g$ 

wherein R is an aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms or COR' wherein R' is a aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms and each OR group is the same or different;

M is a transition metal;

X is independently chlorine, bromine or iodine;

ED is an electron donor;

d is 0.5 to 56;

e is 0, 1, or 2;

f is 2 to 116;

g is >2 and up to 1.5(d)+3; and

- 2) the Lewis Acid of step (5) is
- i) one or more compounds with formula M'(R"n)X(3-n) wherein M' is aluminum or boron; each X is independently chlorine, bromine, or iodine; each R" is independently a saturated aliphatic hydrocarbon radical having 1 to 14 carbon atoms, provided that when M is aluminum, n is 1 to 3 and when M is boron, n is 0 to 1.5; and
- ii) is added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from about 0.1:1 to about 0.3:1 0.10:1 to 1.0:1.
  - 4. (Currently Amended) The process of claim 1-or-2, wherein said Lewis Acid is;
- 1)—one or more alklyaluminum compound(s) with formula  $M'(R''_n)X_{(3-n)}$  wherein M' is aluminum, R" is n-butyl, n-hexyl, n-octyl, iso-octyl, isohexyl, [[and]] or n-decyl, X is Cl or Br and n is a number from 0 to 1.5.; and
- 2) added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 0.75:1.
  - 5. (Currently Amended) The process of claim 4, wherein said Lewis Acid is [[;
- selected from the group consisting of triethylaluminum, tri-n-butyl aluminum, tri-n-hexyl aluminum, tri-n-octyl aluminum, tri n-decyl aluminum, triisoprenyl aluminum,

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dimethyl aluminum chloride, ethylaluminum dichloride, diethylaluminum chloride, and mixtures thereof., and

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- added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 0.30:1.
- 6. (Currently Amended) The process of claim 4 claim 1, wherein the catalyst precursor slurry is partially or fully preactivated by first contacting with diethylaluminum chloride followed by tri-n-hexyl aluminum.
- 7. (Currently Amended) The process of claim 1-or-2-wherein the viscosity of the slurry after addition of the activator or activators in step (5) is adjusted to at least 1500 cP.
- 8. (Currently Amended) The process of claim 1 or 2 in which the slurry of [[(2)]]step (4) is intimately mixed with the Lewis Acid in step (5) by use of one or more vertically disposed static mixers.
- 9. (Currently Amended) The process of claim 1 er-2 wherein the one or more static mixers and connecting piping have length/diameter ratios from 5 to 15.
- 10. (Currently Amended) The process of claim 1 or 2 in which said gas phase reactor is the sole olefin polymerization reactor.
- (Currently Amended) The process of claim 1-or-2 wherein two olefin polymerization reactors are employed.
- 12. (New) The process of claim 1, wherein the catalyst is partially pre-activated in step (5) for about 15 minutes to about 45 minutes prior to the transferring step (6).
- 13. (New) The process of claim 1, wherein a polymer comprising ethylene produced according to the process of claim 1 has a quantity of fines that is at least 10 percent less than the quantity of fines in a polymer produced under a comparative process under the same conditions except that the comparative process does not include the partial pre-activation of the catalyst precursor according to step (5) of the process of claim 1.